

# Ordering-based approaches for improving solver efficiency in reservoir simulation

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## 1. Motivation

Our goal is to improve the efficiency of linear and nonlinear solvers in petroleum reservoir simulators by exploiting physical characteristics intrinsic to the problem:

- Flow is driven by pressure gradients, so an upstream-to-downstream ordering is possible;
- Upwind discretization allows partial resolution of the nonlinear system on a cell-by-cell basis.

## 2. Flow in porous media

The flow of  $n$  immiscible phases in heterogeneous porous media is modelled by  $n$  nonlinear conservation laws defined over  $x \in \mathbb{R}^k$ ,  $1 \leq k \leq 3$ :

$$\frac{\partial(\phi \rho^j S^j)}{\partial t} + \nabla \cdot (\rho^j \mathbf{v}^j) = \rho^j q^j, \quad j = 1, \dots, n, \quad (1)$$

with phase velocities  $\mathbf{v}^j$  given by Darcy's law

$$\mathbf{v}^j = -K \lambda^j(S^1, \dots, S^n) [\nabla p - \rho^j \mathbf{g}]. \quad (2)$$

We close the system with initial and boundary conditions, as well as the *saturation constraint*  $\sum_j S^j = 1$ . The primary variables are  $p$  (pressure) and  $S^j$  for  $j = 1, \dots, n-1$  (saturation). The equations are discretized using:

- Finite volumes with conservative numerical fluxes,
  - Phase-based upwinding for  $\lambda^j(S^1, \dots, S^n)$  (Fig. 3),
  - Implicit time stepping (Backward Euler) for both  $S^j$  and  $p$ .
- The standard nonlinear solver is Newton's method, which is locally quadratically convergent but can diverge for bad initial guesses.

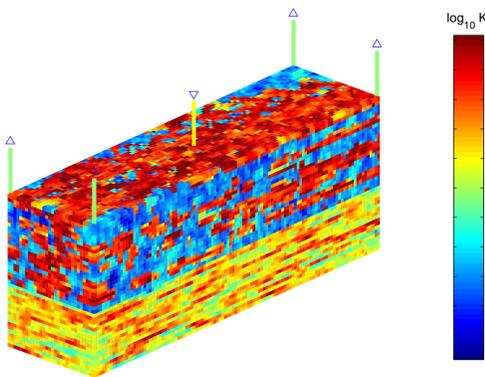


Figure 1: A heterogeneous oil reservoir.

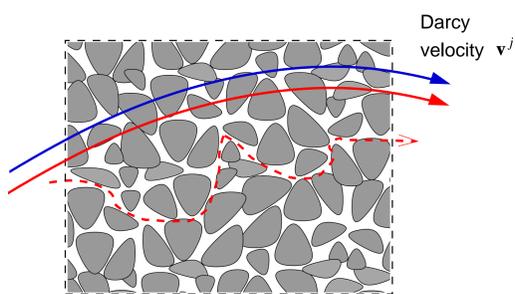


Figure 2: Flow through a porous medium.

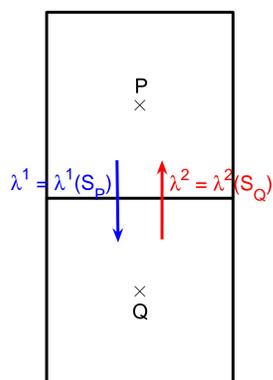


Figure 3: Countercurrent flow.

## 3. Potential ordering

The flow direction of phase  $j$  is completely determined by  $\nabla \Phi^j$ , where

$$\Phi^j = p - \rho^j \mathbf{g}^T \mathbf{x} \quad (3)$$

is the phase potential. If the control volumes are numbered in decreasing order of  $\Phi^j$ , then the upwind discretization ensures

$$f_i^j \text{ is a function of } S_l^j \implies l \leq i. \quad (4)$$

So the residual functions look like

$$\begin{aligned} f_1^j(S_1^j, p_1, \dots, p_N) &= 0 \\ f_2^j(S_1^j, S_2^j, p_1, \dots, p_N) &= 0 \\ &\vdots \\ f_N^j(S_1^j, \dots, S_N^j, p_1, \dots, p_N) &= 0 \end{aligned} \quad (5)$$

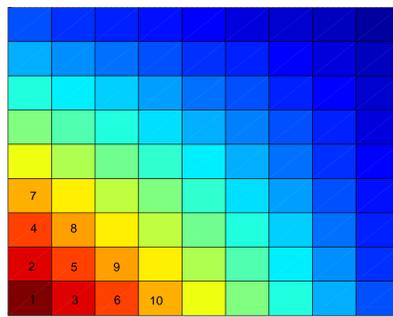


Figure 4: Ordering from highest to lowest potential.

## 4. Reduced-order Newton method

Suppose  $[\partial \lambda^i / \partial S^j]$  is a lower-triangular matrix. Then the residual functions for all phases can be written as

$$\begin{aligned} f_1^1(S_1^1, p_1, \dots, p_N) &= 0 \\ f_2^1(S_1^1, S_2^1, p_1, \dots, p_N) &= 0 \\ &\vdots \\ f_N^1(S_1^1, \dots, S_N^1, p_1, \dots, p_N) &= 0 \\ f_1^2(S_1^1, \dots, S_N^1, S_1^2, p_1, \dots, p_N) &= 0 \\ &\vdots \\ f_N^{n-1}(S_1^1, \dots, S_N^1, \dots, S_1^{n-1}, \dots, S_N^{n-1}, p_1, \dots, p_N) &= 0 \\ f_1^n(S_1^1, \dots, S_N^1, \dots, S_1^{n-1}, \dots, S_N^{n-1}, p_1, \dots, p_N) &= 0 \\ &\vdots \\ f_N^n(S_1^1, \dots, S_N^1, \dots, S_1^{n-1}, \dots, S_N^{n-1}, p_1, \dots, p_N) &= 0. \end{aligned} \quad (6)$$

If  $p_1, \dots, p_n$  are known, we can solve the first  $(n-1) \times N$  equations for  $S_i^j$  by *forward substitution*. Thus, the first  $(n-1) \times N$  equations can be seen as constraints that implicitly define the functions

$$S_i^j = S_i^j(p_1, \dots, p_N). \quad (7)$$

The last  $N$  equations become

$$f_i^n(S(p_1, \dots, p_N), p_1, \dots, p_N) = 0, \quad i = 1, \dots, N. \quad (8)$$

Newton's method is used to solve (8). The resulting method is more efficient because it avoids costly time-step cuts due to non-convergence. Global convergence can be proved for 2-phase incompressible 1D flow without gravity [3]:

1. If the  $\lambda^j$  are uniformly convex, then the reduced Newton method converges globally for **large**  $\Delta t$ ;
2. Suppose the  $\lambda^j$  are convex. Then there exists a set of constraint equations (which can be chosen dynamically) such that the reduced Newton method converges **globally** for all  $\Delta t$ .

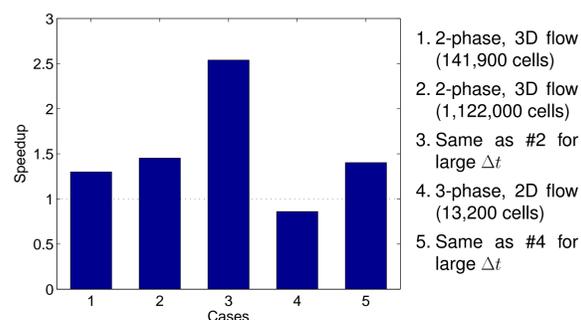


Figure 5: Performance of reduced Newton method [2].

## 5. Linear preconditioning

To solve the linear system within each Newton iteration, iterative methods (e.g. GMRES) are preferred for large-scale (esp. 3D) problems. The Constrained Pressure Residual (CPR) method [1] exploits the saturation-pressure coupling via the two-stage preconditioner

$$M^{-1} = M_2^{-1}(I - AM_1^{-1}) + M_1^{-1}, \quad (9)$$

which is derived from the stationary iteration

$$M_1 x^{(k+1/2)} = (M_1 - A)x^{(k)} + b, \quad (10)$$

$$M_2 x^{(k+1)} = (M_2 - A)x^{(k+1/2)} + b, \quad (11)$$

where

- $M_1$  = Elliptic solve on decoupled pressure system (AMG),
- $M_2$  = Block ILU preconditioner on global system.

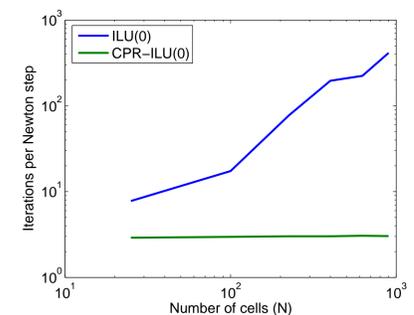


Figure 6: CPR vs. ILU(0) for a simple 2-phase problem.

The above figure shows that CPR is nearly grid-independent, unlike ILU(0). For larger and more complex problems, CPR convergence can be improved by reordering the cells from **upstream to downstream** before computing ILU(0) factors for  $M_2$ . For cocurrent 2-phase flow [3]:

1. A block ILU(0) factorization exists whenever the cells are ordered from upstream to downstream, and it is exact with respect to saturation.
2. If  $L_1, U_1$  and  $L_2, U_2$  are two ILU factors computed based on two topological orderings of the same flow graph, then  $L_1, L_2$  (also  $U_1, U_2$ ) are identical up to permutation.

Hence the ordering is optimal and reduces the sensitivity of CPR with respect to flow configurations, as shown in the examples below.

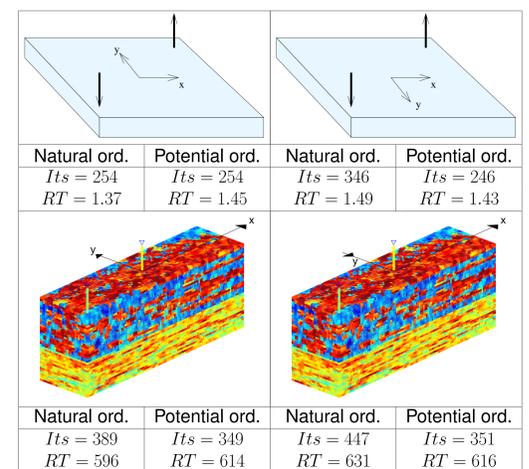


Figure 7: Ordering effects on CPR-ILU preconditioner. Its = Total GMRES its., RT = Running time (sec).

## References

- [1] J. R. Wallis, R. P. Kendall, and T. E. Little. *Constrained residual acceleration of conjugate residual methods*. In Eighth SPE Symposium on Reservoir Simulation, pp. 415–428, 1985.
- [2] F. Kwok and H. Tchelepi. *Potential-based reduced Newton algorithm for nonlinear multiphase flow in porous media*, J. Comput. Phys 227, pp. 706–727, 2007.
- [3] F. Kwok. *Scalable Linear and Nonlinear Algorithms for Multiphase Flow in Porous Media*, PhD thesis, Stanford University, Stanford, CA, Dec. 2007.